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*Patent, Trademark and Copyright Causes*

*Unfair Competition, Trade Secrets,*

*Licensing and Litigation*

*\*Practice limited to Matters and Proceedings*

*before Federal Courts and Agencies; not Admitted*  
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**FORM PTO-1082**

**TRANSMITTAL FOR NEW U.S. PATENT APPLICATION**

Assistant Commissioner of

Patents and Trademarks

Washington, D.C. 20231

Re: New U.S. Patent Application

For: **METHOD OF AND APPARATUS FOR PRODUCING  
PELLETS FROM HEAVY HYDROCARBON LIQUID**

Inventor(s): Yoram BRONICKI  
J. Robert FRIDAY  
Philip B. RETTGER

Attorney Docket: 15155

Sir:

Attached hereto is the application identified above, including:

- 14 Pages Application Consisting of:
- 8 Pages of Textual Specification
  - 2 Pages of 14 Claims
  - 1 Abstract of the Disclosure
  - 3 Sheets of drawings.
  - ☐ Executed Inventor's Declaration
  - ☒ Unexecuted Inventor's Declaration
  - ☐ Small Entity Statement
  - ☐ Assignment and cover sheet
  - ☐ Priority Document

The Government filing fee\* is calculated as follows:

Total Claims . . . . .	<u>14</u> - 20 = <u>0</u>	x \$18.00 = <u>\$0.00</u>
Independent Claims . . . . .	<u>2</u> - 3 = <u>0</u>	x \$78.00 = <u>\$0.00</u>
Base Fee . . . . .		<u>\$690.00</u>
Multiple Dependent Claim Fee (\$260.00) . . . . .		<u>\$ 0.00</u>
Subtotal . . . . .		<u>\$690.00</u>

**TOTAL FILING FEE\***

(accounting for possible small entity status) . . . **\$690.00**



07/27/00

BOX PATENT APPLICATION  
Attorney Docket No. 15155JC759 U.S. PTO  
09/627166  
07/27/00

## IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Application of:

Yoram BRONICKI  
J. Robert FRIDAY  
Philip B. RETTGER

Serial No. NOT YET ASSIGNED

Filed: July 27, 2000

For: **METHOD OF AND APPARATUS FOR PRODUCING PELLETS FROM HEAVY  
HYDROCARBON LIQUID**TRANSMITTAL LETTERThe Assistant Commissioner for Patents  
Washington, D.C. 20231

Sir:

Submitted herewith for filing in the U.S. Patent and Trademark  
Office is the following:

- (1) Transmittal Letter
- (2) PTO Form-1082
- (3) 14 page Application consisting of:
  - 8 pages Textual Specification
  - 2 pages of 14 claims
  - 1 page containing the Abstract of the Disclosure
  - 3 sheets drawings
- (4) Unexecuted Declaration/Power of Attorney
- (5) Postcard for early notification of serial number.

Respectfully submitted,

NATH &amp; ASSOCIATES PLLC

By: Gary M. Nath  
Registration No. 26,965  
Jerald L. Meyer  
Registration No. 41,194  
Customer No. 20529Date: July 27, 2000  
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GMN/JLM/dd:APPL.trans

\_\_\_ \*Reduced by one-half, as applicant(s) is/are a "small entity".  
A Declaration Claiming Small Entity Status:

\_\_\_ is submitted herewith;

\_\_\_ will be filed at a later date.

\_\_\_ Foreign priority is claimed under 35 U.S.C. § 119 from KOREA  
Patent Application(s) No. \_\_\_\_\_ dated \_\_\_\_\_.

\_\_\_ Priority document(s) will be submitted at a later date.

\_\_\_ Priority document(s) is/are submitted herewith.

X Executed Declaration(s) will be submitted at a later date  
pursuant to 37 CFR § 1.41 and § 1.53, with an appropriate  
surcharge under 37 CFR § 1.16(e).

X Formal drawing(s) is/are attached.

\_\_\_ Formal drawing(s) will be submitted at a later date.

\_\_\_ Assignment document(s) is/are submitted herewith; the recorda-  
tion fee of \$40.00 per document is enclosed herewith.

\_\_\_ Assignment document will be submitted at a later date.

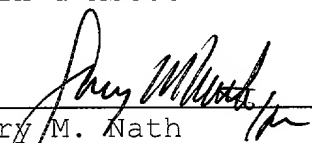
\_\_\_ A Verified Translation will be submitted at a later date.

X No payment is enclosed at this time. Full payment will be  
made when the executed Declaration is submitted.

\_\_\_ Submitted herewith is a check in the amount of \$ \_\_\_\_\_.

Respectfully submitted,

**NATH & ASSOCIATES PLLC**

  
\_\_\_\_\_  
Gary M. Nath  
Registration No. 26,965  
Jerald L. Meyer  
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Date: July 27, 2000  
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GMN/JLM/dd (1082)

METHOD OF AND APPARATUS FOR PRODUCING PELLETS FROM HEAVY  
HYDROCARBON LIQUID  
DESCRIPTION

1. Technical Field

This inventions relates to processing heavy hydrocarbon feeds which may be used in refineries and/or producing power, and more particularly, to a method of and apparatus for producing pellets of heavy hydrocarbon feeds such as residual oil and/or asphaltenes.

2. Background of the Invention

A typical petroleum refinery receives crude oil and primarily produces gasoline, jet fuel, diesel fuel, and heating oil. The by-products of the refinery process are light gases, and heavy, viscous residual oil sometimes referred to as vacuum residual. The light gases can be used in the refinery, or sold outside the refinery as fuel.

To store, transport, and thus dispose of the heavy residual oil, it is conventional to reduce its viscosity by mixing it with lower viscosity diluent such as diesel fuel produced by the refinery. The resultant residual fuel oil is usually sold as fuel to electric utilities.

Disposing of residual oil by blending with valuable diluent is not always cost effective; and in many refineries, solvent deasphalting processing of the residual oil is carried out to produce charge stock for catalytic cracking, or hydrocracking units, and thus to reduce the amount of less valuable by-products. Such processing involves mixing the residual oil with a light hydrocarbon solvent, such as propane, iso-butane, normal-butane, iso-pentane, normal-pentane, or mixtures of these hydrocarbons. When a light hydrocarbon solvent is mixed with the residual oil under conditions of high pressure and temperature in an equilibrium vessel, the residual oil separates into two

distinct fractions; a deasphalted oil (DAO) fraction essentially free of asphaltenes, and an asphaltene fraction containing a small portion of deasphalted oil which is soluble in this fraction. By providing additional equilibrium vessels, intermediate products can be produced which are not as "clean" as the DAO, but which are "cleaner" than the asphaltenes.

Many situations require the asphaltene, that is usually quite hot (sometimes as high as about 450°F), to be transferred or transported to another location near or in the refinery. Transporting asphaltene at such temperatures is not a simple procedure since it may need the use of costly heat insulators.

On the other hand, to solidify the asphaltene is very complicated and usually involves costly machinery. Moreover, transportation of such solidified heavy hydrocarbon material is also quite expensive and usually brings with it heavy maintenance costs.

It is therefore an object of the present invention to provide a new and improved method of and apparatus for processing heavy hydrocarbon feeds such as residual oil and/or asphaltene and producing pellets therefrom wherein the disadvantages as outlined are reduced or substantially overcome.

#### SUMMARY OF THE INVENTION

Apparatus for processing heavy hydrocarbons or asphaltene and producing pellets from hot heavy hydrocarbon or asphaltene, in accordance with the present invention, comprises flow means that supplies the hot heavy hydrocarbon or asphaltene through a conduit to its outlet; and pellet producing medium or means that breaks up the liquid stream of the hot asphaltene exiting the outlet of the conduit and produces pellets of asphaltene. Furthermore, the apparatus comprises a reservoir or container that collects the pellets of heavy hydrocarbon or asphaltene together with some fluid producing a slurry; and transporting

means that transports the slurry to the required location. Preferably, the fluid is liquid water. In addition, the pellet producing medium preferably is liquid water.

Furthermore, the present invention provides a method that processes heavy hydrocarbons or asphaltene and produces pellets from hot heavy hydrocarbon or asphaltene, the method comprising the steps of: supplying the hot heavy hydrocarbon or asphaltene through a conduit to its outlet; and breaking up the liquid stream of hot asphaltene exiting the outlet of the conduit using a pellet producing medium to produce pellets of heavy hydrocarbon or asphaltene. The pellets of heavy hydrocarbon or asphaltene are collected in a reservoir or container together with some fluid producing a slurry; and the slurry is transported to a required location. Preferably, the step of collecting the pellets in a reservoir or container together with some fluid producing a slurry is carried out by collecting the pellets in a reservoir or container together with some liquid water producing a slurry. In addition, the step of breaking up the liquid stream of hot asphaltene flowing out of the outlet of the conduit using a pellet producing medium to produce pellets of heavy hydrocarbon or asphaltene is preferably carried out by breaking up the liquid stream of hot asphaltene flowing out of the outlet of the conduit using liquid water to produce pellets of heavy hydrocarbon or asphaltene.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Embodiments of the present invention are described by way of example, and with reference to the accompanying drawings wherein:

Fig. 1A is a block diagram of an oil refinery designed to produce, from the residual oil, an asphaltene/solvent stream and a deasphalted oil/solvent stream;

Fig. 1B is a block diagram of a conventional evaporative solvent recovery section of a solvent deasphalting unit which

receives an asphaltene/solvent stream and a deasphalted oil/solvent stream and recovers the solvent, and produces product in the form of asphaltene, and deasphalted oil;

Fig. 2 is a block diagram of an embodiment of the present invention for processing a hydrocarbon feed;

Like reference numerals and designations in the various drawings refer to like elements.

#### Detailed Description

Referring now to Fig. 1A, reference numeral 1 designates a typical petroleum refinery that receives crude oil and primarily produces gasoline, jet fuel, diesel fuel, and heating oil. Light gases, which are a by-product of the refinery process are typically sold, or used outside the refinery as fuel. Heavy, viscous residual oil, sometimes referred to as vacuum residual, are also by-products, and are typically converted to residual fuel and sold to electric utilities by blending with diesel fuel to reduce viscosity. The broken lines connecting the diesel fuel output of the refinery to the residual oil output indicate this blending process.

An alternative way to dispose of the residual oil is to utilize a solvent deasphalting unit which involves mixing the residual oil with a light hydrocarbon solvent in a separator to form a mixture that separates into a product stream of asphaltene/solvent and a product stream of deasphalted oil/solvent. The solvent deasphalting unit includes a solvent recovery section that is effective to remove substantially all of the solvent from the product streams, thus recovering the solvent which is returned to the deasphalting unit.

The solvent recovery unit may utilize a supercritical solvent recovery process to remove a great deal of solvent from the DAO product stream; the balance of the solvent being removed by an evaporative solvent recovery process operating on the heavy

and any intermediate product streams and the DAO product stream produced by the supercritical solvent recovery process. If supercritical solvent recovery were not used as the primary means to recover solvent from the DAO, an evaporative solvent recovery process would operate on all of the product streams.

An evaporative solvent recovery process, which operates on the streams produced as described above conventionally, is shown by reference numeral 10 in Fig. 1B, and is applicable to solvent recovery systems using supercritical and subcritical solvent recovery, or only subcritical solvent recovery. Such process recovers the solvent so that it can be used again, and produces a product stream of asphaltene, and a product stream of DAO. The DAO fraction is recycled back to the refinery for conversion to gasoline, jet fuel, diesel fuel, and heating oil. The asphaltene fraction may be blended with a lighter, lower viscosity diluent such as diesel fuel, and converted to residual oil for sale to utilities, or in some cases, sold as solid fuel. For light solvent deasphalting units such as propane, where residual solvent is recovered below the pressure of the solvent drum, the vaporized solvent from the strippers has to be repressurized to the pressure of the solvent drum before being condensed.

Numeral 100 in Fig. 2 designates an embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention wherein heavy hydrocarbon or asphaltene feed is conveyed via conduit 102. E.g. heavy hydrocarbon or asphaltene feed can be supplied in line 31 with or without the use of a pump coming from the final asphaltene separation vessel. Often, the asphaltene product in line 31 can be quite hot (sometimes as high as about 450°F). As the heavy hydrocarbon or asphaltene exits outlet 104 of conduit 102, it meets a pellet producing means or pellet producing media, e.g. gas, liquid, or mechanical device. When a liquid is used the pellet producing media exits conduit



106 via outlet 108. When a gas or mechanical device is used for producing pellets, a cooling and transporting liquid can be added via e.g. conduit 106. The pellet producing means or pellet producing media breaks up the heavy hydrocarbon or asphaltene liquid stream and the heavy hydrocarbon or asphaltene solidifies into pellets 110 as it cools. Reduction in pellet or solid particle size can be achieved by controlling the shear forces induced by the liquid exiting conduit 106 via use of an appropriate flow rate or flow channel geometry. Pellets 110 thus produced together with fluid 111 produce slurry 114. Slurry 114 can flow in a channel or collect in reservoir or container 112 containing some or substantially all of liquid exiting outlet 108 of conduit 106. Bottom 109 of reservoir or container 112 is preferably inclined to ensure the flow of slurry 114 in the direction from the end of reservoir or container 112 adjacent outlet 108 of conduit 106 to the end of reservoir or container 112 near pump 116. The resulting heavy hydrocarbon or asphaltene - fluid slurry is then supplied to conduit 115 using pump 116. Pump 116 can be selected to provide additional size reduction (crushing) or such additional size reduction means can be added separately. In such a manner, the heavy hydrocarbon or asphaltene pellets or solid particles present in conduit 115 are transported to location 118. At location 118, the heavy hydrocarbon or asphaltene - fluid slurry can be treated by removing the fluid from the asphaltene e.g. separating the fluid by using separator 120, so that the heavy hydrocarbon or asphaltene is prepared for use or storage. The separated fluid can be recycled to conduit 106 via conduit 122. If required, a fines separation and remelting element can be added immediately before location 118 or as part of separator 120.

Preferably, the present invention is carried out in a controlled environment or surroundings or even more preferably in an enclosure.

In accordance with the present invention, the pellet producing media and transporting fluid is fluid in which the heavy hydrocarbon or asphaltene does not dissolve therein. For use with heavy hydrocarbons or asphaltene, water is particularly suitable and is the preferred pellet producing media as well as the preferred transporting fluid.

In addition, when, according to the present invention, the pellet producing media is gas, then high velocity air or an other inert gas can be used. Moreover, when, according to the present invention, a pellet producing means is used, e.g. a mechanical device such as a rotating disc, blade(s) or ribbon(s) can be used. When such mechanical devices are used, the use of a cooling or transportation medium is very important.

Additionally, in accordance with the present invention, pellet producing can be carried out by pellet producing means or pellet producing medium either before or after contact with the cooling medium and the commencement of solidification. Thus, in accordance with the present invention, the fluid can meet the heavy hydrocarbon or asphaltene such that a jet of fluid, e.g. a water jet meets the heavy hydrocarbon or asphaltene prior to the pellets falling into reservoir 112. Alternatively, the fluid can meet the heavy hydrocarbon or asphaltene in a reservoir of fluid, e.g. such that the heavy hydrocarbon or asphaltene falls into the reservoir of fluid e.g. water in container 112. In such a case, the jet of water meets the asphaltene below the surface of the slurry 114 present in reservoir or container 112.

Moreover, rather than transporting the heavy hydrocarbon or asphaltene - fluid slurry on line, the heavy hydrocarbon or

asphaltene slurry may first of all be stored before it is transported to the required location.

Also, while heavy hydrocarbon or asphaltene is mentioned in this specification as material from which pellets can be produced in accordance with the present invention, other materials, e.g. vacuum residue, etc. can be considered as material from which pellets can be produced in accordance with the present invention.

In addition, it should be noted that supply means or lines mentioned in this specification refer to suitable conduits, etc.

Moreover, it should be pointed out that while this specification presents Figs. 1A and 1B as apparatus and a method for producing asphaltenes, pellets can be produced in accordance with the present invention from asphaltene produced in any other method and by any other means.

Additionally, while the term asphaltene is used throughout the specification, the term asphaltene is taken to include in its meaning asphalt like materials that are predominately pentane insoluble.

Furthermore, it should be pointed out that the present invention includes as well the method for operating the apparatus disclosed with reference to above-described figures.

It is believed that the advantages and improved results furnished by the method and apparatus of the present invention are apparent from the foregoing description of the invention. Various changes and modifications may be made without departing from the spirit and scope of the invention as described in the claims that follow.

WHAT IS CLAIMED IS:

1. Apparatus for producing asphaltene pellets comprising:
  - a) flow means that supplies hot asphaltene through a conduit to its outlet; and
  - b) pellet producing medium that breaks up the liquid stream of said hot asphaltene exiting the outlet of said conduit and produces pellets of asphaltene.
2. Apparatus according to claim 1 including:
  - a) a reservoir or container that collects said pellets of asphaltene together with some fluid producing a slurry; and
  - b) transporting means that transports said slurry to the required location.
3. Apparatus according to claim 1 wherein said fluid is liquid water.
4. Apparatus according to claim 3 wherein said transporting means includes a conduit that supplies the slurry to the required location.
5. Apparatus according to claim 3 including a pump for pumping the slurry to said location.
6. Apparatus according to claim 1 wherein said pellet producing medium is liquid water.
7. A method for producing asphaltene pellets comprising the steps of:
  - a) supplying hot asphaltene through a conduit to its outlet; and
  - b) breaking up the liquid stream of said hot asphaltene exiting the outlet of said conduit using a pellet producing medium to produce pellets of asphaltene.

8. A method according to claim 7 further comprising the steps of:

- a) collecting said pellets of asphaltene in a reservoir together with some fluid producing a slurry; and
- b) transporting said slurry to a required location.

9. A method according to claim 8 wherein the step of collecting said pellets of asphaltene in a reservoir together with some fluid producing a slurry is carried out by collecting said pellets of asphaltene in a reservoir together with some liquid water producing a heavy hydrocarbon or asphaltene - water slurry.

10. A method according to claim 7 wherein said step of breaking up the liquid stream of said hot asphaltene flowing out of the outlet of said conduit using a pellet producing medium so that pellets of asphaltene are produced is carried out by spraying a fluid so that the fluid contacts the asphaltene exiting said outlet of the conduit and pellets of asphaltene are produced.

11. A method according to claim 9 wherein the step of transporting said slurry to a required location is carried out by supplying said slurry via a conduit to a required location.

12. A method according to claim 11 including pumping the slurry to said location.

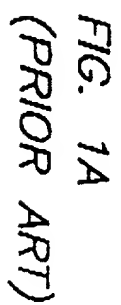
13. A method according to claim 10 wherein the step of spraying a fluid so that the fluid contacts the asphaltene exiting said outlet of the conduit and pellets of asphaltene are produced is carried out by spraying liquid water.

14. A method according to claim 8 including grinding said asphaltene pellets and transporting the grinded asphaltene pellets to a location.

METHOD OF AND APPARATUS FOR PRODUCING PELLETS FROM HEAVY  
HYDROCARBON LIQUID

Abstract

Apparatus for producing pellets from hot heavy hydrocarbon or asphaltene, in accordance with the present invention, includes flow means that supplies the hot heavy hydrocarbon or asphaltene through a conduit to its outlet; and pellet producing medium or means that breaks up the liquid stream of the hot asphaltene flowing out of the outlet of the conduit and produces pellets of asphaltene. Furthermore, the apparatus includes a reservoir or container that collects the pellets of heavy hydrocarbon or asphaltene together with some fluid producing a slurry; and transporting means that transports the slurry to the required location. Preferably, the fluid is liquid water. In addition, the pellet producing medium preferably is liquid water.



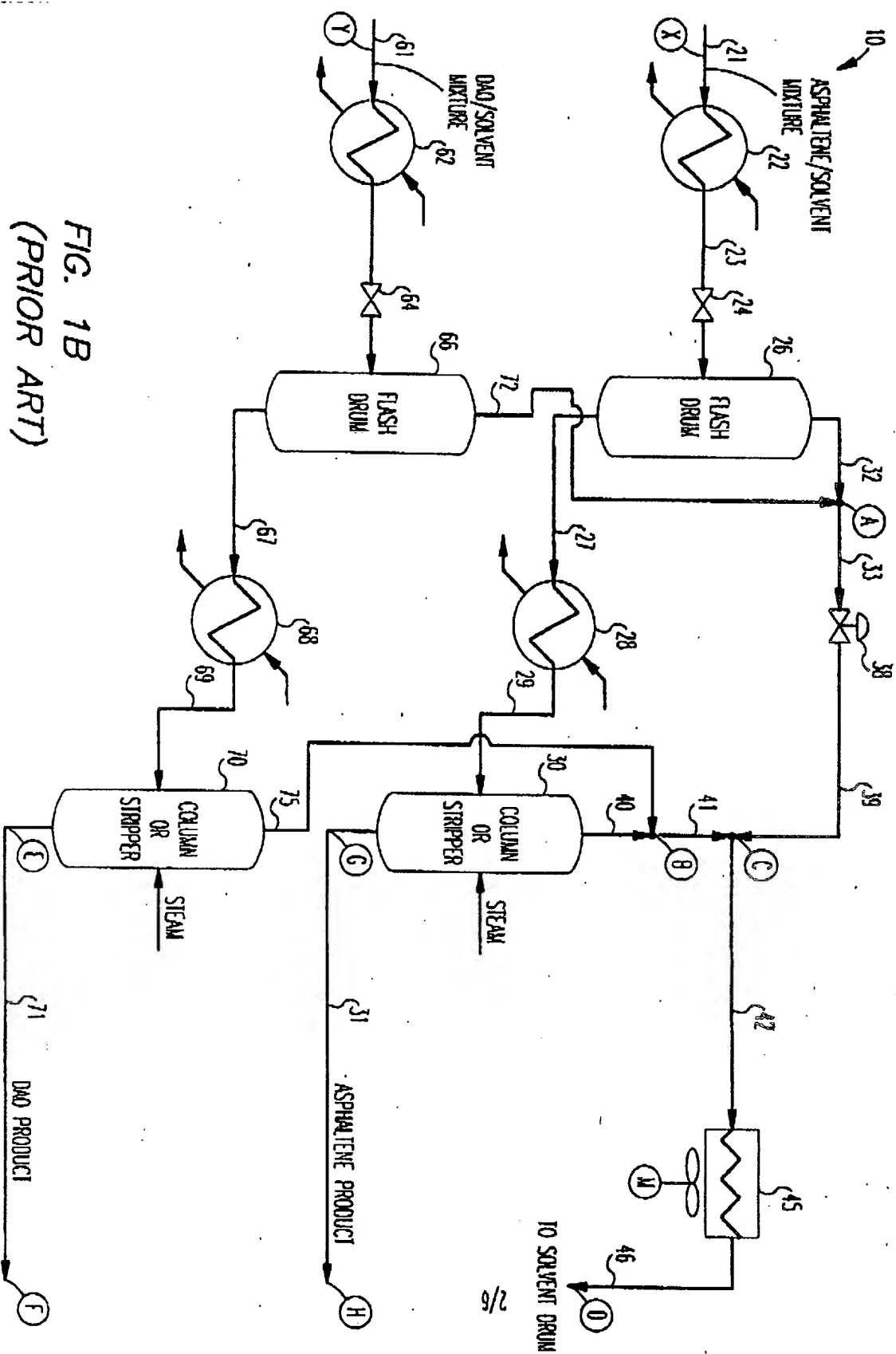


FIG. 1B  
(PRIOR ART)





## DECLARATION FOR PATENT APPLICATION

Attorney Docket: 15155  
Page 1 of 2

As a below-named inventor(s), I/we hereby declare that:

My/Our residence(s), post office address(es) and citizenship(s) is/are as stated below next to my/our name(s).

I/We believe I/we am/are the original inventor, first and sole (if only one name is listed below) or the original, first and joint inventors (if plural names are listed below) of the subject matter which is claimed, and for which a patent is sought on the invention entitled:

**METHOD OF AND APPARATUS FOR PRODUCING PELLETS FROM HEAVY HYDROCARBON LIQUID**

the specification of which: (check one)

☒ is attached hereto.

☐ was filed on \_\_\_\_\_, as Serial No. \_\_\_\_\_,

and was amended on \_\_\_\_\_ (if applicable).

We hereby state that we have reviewed and understand the contents of the above-identified specification, including the claims, as amended by any amendment referred to above.

We acknowledge the duty to disclose information which is material to the patentability of this application as defined by 37 CFR § 1.56.

We hereby claim foreign priority benefits under 35 U.S.C. § 119 of any foreign application(s) for patent or inventor's certificate listed below, and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

Prior Foreign Applications:

(Application No.)	(Country)	(Day/Month/Year Filed)	Priority Claimed	
			<input type="checkbox"/> Yes	<input type="checkbox"/> No
_____ (Application No.)	_____ (Country)	_____ (Day/Month/Year Filed)	<input type="checkbox"/> Yes	<input type="checkbox"/> No
_____ (Application No.)	_____ (Country)	_____ (Day/Month/Year Filed)	<input type="checkbox"/> Yes	<input type="checkbox"/> No
_____ (Application No.)	_____ (Country)	_____ (Day/Month/Year Filed)	<input type="checkbox"/> Yes	<input type="checkbox"/> No

We hereby appoint Gary M. Nath, Reg. No. 26,965; Harold L. Novick, Reg. No. 26,011; Todd L. Jeanneau, Reg. No. 40,669; Lee C. Heiman, Reg. No. 41,827; Jerald L. Meyer, Reg. No. 41,194; Joshua B. Goldberg, Reg. No. 44,126; David R. Murphy, Reg. No. 22,751; Paul A. Sacher, Reg. No. 43,418; Charles D. Niebylski, Reg. No. 46,116; Deborah H. Yellin, 45,904; Nahied K. Usman, Reg. No. P-47,148; and Roger Haan, Reg. No. 46,376; as my attorneys to prosecute this application and transact all business in the U.S. Patent and Trademark Office connected therewith.

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We hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by 35 U.S.C. § 112, first paragraph, I/we acknowledge the duty to disclose material information as defined in 37 CFR § 1.56 which occurred between the filing date of the prior application and the national or PCT international filing date of this application:

(U.S. Application Serial No.) (U.S. Filing Date) (Status--patented, pending, abandoned)

(U.S. Application Serial No.) (U.S. Filing Date) (Status--patented, pending, abandoned)

DECLARATION FOR PATENT APPLICATION

Attorney Docket: 15155  
Page 2 of 2

We hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements are made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under 18 U.S.C. § 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Full name of sole or first inventor: Yoram BRONICKI

Inventor's Signature \_\_\_\_\_ Date \_\_\_\_\_

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Country of Citizenship: ISRAEL

Post Office Address: same as residence

Full name of second inventor: J. Robert FRIDAY

Inventor's Signature \_\_\_\_\_ Date \_\_\_\_\_

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Country of Citizenship: U.S.A.

Post Office Address: same as residence

Full name of third inventor: Philip B. RETTGER

Inventor's Signature \_\_\_\_\_ Date \_\_\_\_\_

Residence: 2438 Shannon Drive, Walnut Creek, CA 94598, U.S.A.

Country of Citizenship: U.S.A.

Post Office Address: same as residence